

# Lecture 22, Oct 27, 2022

## Forces on a Fluid

- Two categories:
  - Body forces: developed without physical contact, proportional to the fluid's mass
    - \* e.g. gravity
  - Surface forces: developed with physical contact at the surface of a fluid element
    - \* These don't have to be real surfaces
    - \* Can be broken down into components tangential (shear) or normal to the surface
    - \* Surface forces result in stresses

### Definition

Normal stress is defined as

$$\sigma = \lim_{\delta A \rightarrow 0} \frac{\delta F_n}{A}$$

Shear stress is defined as

$$\tau = \lim_{\delta A \rightarrow 0} \frac{\delta F_t}{\delta A}$$

- Stress: Force per unit area
  - Stress at a point is defined as the limit as the area decreases to 0
  - Normal stress is defined as  $\sigma = \lim_{\delta A \rightarrow 0} \frac{\delta F_n}{A}$
  - Shear stress is defined as  $\tau = \lim_{\delta A \rightarrow 0} \frac{\delta F_t}{\delta A}$
  - Since there are multiple surfaces that can pass through a point, the stress at a point is described completely by specifying 3 stresses on mutually perpendicular planes through the point
- Double subscript notation for stress:  $\tau_{xy}$  is a stress on the  $x$  plane (unit vector in the  $x$  direction) acting in the  $y$  direction
  - One normal stress  $\sigma_{xx}$ , two tangential stresses  $\tau_{xy}, \tau_{xz}$ , for every surface (in this case  $x$ )
  - This means there are 9 such stresses for every point! From these we can form a stress tensor to describe all stress components:
- Stress tensor: 
$$\begin{bmatrix} \sigma_{xx} & \tau_{xy} & \tau_{xz} \\ \tau_{yx} & \sigma_{yy} & \tau_{yz} \\ \tau_{zx} & \tau_{zy} & \sigma_{zz} \end{bmatrix}$$

## (Dynamic) Viscosity

- Recall shear stress in a solid is proportional to deformation angle  $\delta\alpha$
- Since a fluid never stops deforming, shear stress is instead proportional to the rate of change in the deformation angle
  - $\tau \propto \frac{d\alpha}{dt}$
- In a parallel flow field with a velocity gradient (e.g. a boundary layer), the fluid undergoes shear forces as it deforms due to difference in velocity between layers
  - $d\alpha = \frac{du}{dy} dt \implies \frac{d\alpha}{dt} = \frac{du}{dy}$
  - The rate of angular deformation of the fluid region is equal to the velocity gradient of the field
- Since  $\tau \propto \frac{d\alpha}{dt} = \frac{du}{dy}$  for Newtonian fluids we can let  $\tau = \mu \frac{d\alpha}{dt} = \mu \frac{du}{dy}$ , where the proportionality constant  $\mu$  is the *viscosity*

### Definition

The viscosity of a Newtonian fluid is  $\mu$  defined such that

$$\tau = \mu \frac{d\alpha}{dt} = \mu \frac{du}{dy}$$

where  $\frac{d\alpha}{dt}$  is the rate of angular deformation of the fluid element, equal to  $\frac{du}{dy}$ , the velocity gradient in the fluid

- Newtonian fluids' viscosity are independent of the rate of deformation
  - On a graph of shear stress vs. velocity gradient, a Newtonian fluid starts at the origin and has constant slope
  - For non-Newtonian fluids, this graph is nonlinear and  $\mu$  can vary with rate of deformation; some may even not start at the origin
    - \* Shear thinning: with higher rates of deformation, viscosity decreases (e.g. some paints, blood, cookie dough)
    - \* Shear thickening: with higher rates of deformation, viscosity increases (e.g. cornstarch + water)
    - \* Bingham plastic: acts like a solid until a certain shear stress, until a certain threshold after which it acts like a fluid (e.g. toothpaste)
      - Graph starts above zero
  - The *local viscosity/apparent viscosity*  $\mu_{ap}$  is  $\mu$  at the local conditions
- Viscosity has a strong dependence of temperature:
  - For liquids, viscosity *decreases* with temperature
    - \* Viscosity is caused by intermolecular forces; at higher temperatures molecules overcome these forces
  - For gases, viscosity *increases* with temperature
    - \* Viscosity is caused by molecular collisions; at higher temperatures molecules collide more
- “Viscosity” commonly refers to dynamic viscosity as opposed to kinematic viscosity

### Definition

The kinematic viscosity  $v = \frac{\mu}{\rho}$ , where  $\mu$  is the dynamic viscosity and  $\rho$  is the density

## Compressibility

### Definition

The bulk modulus is defined as  $E_V = -\frac{1}{\mathcal{V}} \frac{dP}{d\mathcal{V}}$  where  $\mathcal{V}$  is the volume

- Bulk modulus measures compressibility; the larger it is, the less compressible the fluid
  - Note an increase in  $P$  causes a decrease in  $\mathcal{V}$ , which is why there is a negative sign
  - Alternatively can be expressed as  $E_V = \frac{1}{\rho} \frac{dP}{d\rho}$  (note there is no minus sign)
    - \*  $m = \rho\mathcal{V} \implies dm = \rho d\mathcal{V} + \mathcal{V}d\rho = 0 \implies \frac{d\rho}{\rho} = -\frac{d\mathcal{V}}{\mathcal{V}}$
  - A truly incompressible flow has  $E_V \rightarrow \infty$ 
    - \* For water it is  $2.2 \times 10^9$  Pa, so it can be approximated as incompressible
    - \* Even though air is a lot more compressible, we can still assume it to be incompressible in a low speed flow